

AMENDMENTS TO THE SPECIFICATION

On page 9, please replace the paragraph bridging pages 9 and 10 with the following:

At the pH adjusting tank 6 of the ammonia recovery system, the pH is adjusted to 9-12 with an aqueous sodium hydroxide solution 26 to facilitate precipitation of the Ca portion of the filtrate 25 in the precipitation/separation tank 8. This pH condition not only facilitates precipitation and separation of the Ca but also facilitates dissipation of the ammonia in the stripper 9. A liquid containing an aqueous carbonic acid solution 27 is also supplied at the pH adjusting tank 6 for precipitation and separation of the Ca portion. The liquid leaving the pH adjusting tank 6 is supplied to the flocculation reaction tank 7 where it is mixed with a coagulant 28. The liquid leaving the flocculation reaction tank 7 is supplied to the precipitation/separation tank 8, where salts including calcium carbonate and heavy metals are precipitated and separated, and are discharged from the bottom of the precipitation/separation tank 8 out of the system as solids 30. Next, the supernatant 29 is supplied to the stripper 9, and steam 32 is blown in from the bottom of the stripper 9, ammonia 31 is recovered as an aqueous solution at the top of the stripper column while ammonia is also removed from the bottom of the column and the nitrogen portion is discharged out of the system as waste water 33 meeting waste water regulations.